

FireFOAM to Model inside Battery Thermal Disorder Propagation



10th FM Global Open Source CFD Fire Modeling Workshop, Norwood MA on May 30 - 31, 2018.



Some words about the context

Energy storage is becoming a critical issue

- For stationary applications (renewable generation plants, electric grids, ...)
- For various mobile applications (cars, electronic devices, ...)
- Current Lithium Ion Batteries (LIBs) are more & more used

For all cases, autonomy is a key

- Energy density is increasing → compacity increases
- Battery size is more and more important
- Safety is still highly important





From the individual cells



Through the module







Safety is commonly addressed using experiments

- Individual cell behavior depending on the chemistry
 - Crash, stability, impact, overcharge, ...
 - Gas production, HRR and other measurements
- Lots of data are available regarding battery testing

The current very large batteries require an innovative approach

- With very large experimental facilities ... up to a certain limit (20 MW in INERIS)
- Using numerical modelling





Several steps to be modelled

- 1. Ignition in one cell
 - Several complex physical phenomena
 - Depending on the ignition source (internal short-circuit, overcharge, ...)
- 2. Gas release and ignition
 - Mixture of several flammable gases (EC / DMC / ...)
- 3. Temperature rise in the surrounding
 - Combustion of the emitted gases
 - Strong interaction with the air flow and battery structure opening
- 4. Other cells runaway
 - Assuming other cells will be ignited by thermal runaway
 - Evaluation of the internal temperature
- 5. Neighbor cells burning
 - Similar to the initial burning cell



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As usual, ignition is very complex

- Cell ignition depends on the source
 - Short-circuit, overcharging, structural damages, ...
 - Clearly impossible to consider each kind of possible sources
- Hopefully, during the propagation process
 - Ignition mechanism is based on thermal effect





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Ignition is a phenomenon governed by inner cell behavior

→ We decided not to model phenomena inside the cell

Ignition is considered to occur at a given time

• The HRR from the first cell is fixed thanks to experimental data

This requires

- An experiment at cell scale with HRR measurement
- An experimental control of the failure mode



Electrolyte is composed of several chemicals

- Mixtures of
 - ethylene carbonate (EC) $C_3H_4O_3$
 - dimethyl carbonate (DMC) $C_3H_6O_3$
 - ethyl methyl carbonate (EMC) $C_4H_8O_3$
 - diethyl carbonate (DEC) $C_5H_{10}O_3$
 - ... + Lithium salt (LiPF₆)



• Individual mixture test at lab scale (FPA) using CDG and OC calorimetry

Definition of the chemical reaction to be used

- LP50 case : EC/EMC (1/1, wt/wt) + 12,2%wt of LiPF6, neglected
- 1.14 $C_3H_4O_3$ + 0.96 $C_4H_8O_3$ + 7.16 $(O_2$ + 3,72 N_2) → 7.3 CO_2 + 6.12 H_2O + 26.6 N_2
- Average value: $\Delta Hc \approx 16 \text{ kJ/g}$
- A simplified reaction used as a first approach

 $C_3H_4O_3 + 5/2 (O_2 + 3.72 N_2) \rightarrow 3 CO_2 + 2 H_2O + 9.3 N_2$



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Then a model can be built

Considering the cell geometry

• **Cylinder**; Pouch; Prismatic

With a gas injection boundary condition

- Gas flow designed to reproduce the measured HRR
- Based on the chemical reaction and the ΔHc

Considering the chemical product and reaction







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Fire behavior comparison in an open field, unfortunately

• Battery tests are not designed for CFD code validation

The flame is 3 times longer than the cell and as large as the module

- Flame length is quite correct
- Temperature is in the correct order of magnitude
- But how is representative the boundary condition?





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But inside a module the flame geometry is complex



The cell opening mode is crucial

- The whole back face
- A part of the back face
- An opening along the external surface



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With consequently strong fire differences

Slice for underneath cells

- Fire impinges several cells at the bottom
- Cells are mainly heated by the bottom face

Open at the back of one cell

- Fire impinges the back of the module
- Surrounding cells are heated at their back
- Some cells are heated by the top



1.550e+03 1230.8 911.5 592.25 2.730e+02

1550e+03

1230.8

911.5

592.25

2.730e+02

Requirement of dedicated boundary conditions

- To consider the heating of the surrounding cells
- To evaluate their ignition delay



Such an approach requires first

- To take into account the geometry of the battery
- To consider the geometry of the fire → the opening mode of the cell
- To have a correct prediction of the HRR and, consequently, of the temperature



The first step: Energy given to the cell

Based on the temperature distribution

- Evolution on the cells surface along time
- Enables computation of the inner cell temperature



A very simple approach

- When the temperature reaches 155°C → cell turns into fire
- Simple to model but does not consider the specific cell volume

The considered approach

- Energy received by the cell is used to heat the electrolyte (mC_p Δ T)
- When the inner cell temperature reaches 155°C → cell turns to fire
- Does not consider the electro-chemical parameters
 - → To be introduced later
- Initial temperature is a critical parameter (20°C, 50°C, 80°C?)



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But non only

Cells are located into a module

Modules are placed into the LIB

Fire ventilation is a fundamental issue

- The initial available oxygen
- The vent behavior
 - Opening based on T and P
- The cell structure breakage
 - Criteria requirement







Several steps

- Surface temperature computation
- Evaluation of the inner material temperature increase considering thermophysical properties and thickness
- When the structure resistance reached 30% of the initial value, structure to be open (BC modification)







Achieved

- First evaluation of the FireFOAM capability
 - Geometry, chemistry, ...
- Evaluation of the input hypothesis
 - Nature of the cell opening, HRR, ...

To be done

- Confinement opening because of the temperature rise
- Module to module propagation
- Thermal protection influence evaluation



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